

> restart;

Supplementary Code for "Lubhani Mishra *et al* 2021 *J. Electrochem. Soc.* **168** 092502"

NOTE:

Correction: The definition of the Peclet number (Pe) has been modified to:

$$Pe = (Mw * i_0 * L) / (\rho * F * D)$$

Caveats:

This code takes the final form of the model after Landau transformation.

The model solves the PDEs for concentration and potential using numerical method of lines.

A 3 point forward/backward difference is used at the boundaries for first derivatives. Second order central difference is used in the spatial direction for second derivatives. A cell-centered finite difference/finite volume method may be more robust for general discretization of PDEs. In general, when convection (or first derivatives are involved) proper upwind schemes may be needed. N = 10 internal nodes points are used for demonstration. Higher number of node points may be needed for convergence.

This code is not optimized for speed/efficiency/memory usage.

The same model can be solved more efficiently using collocation in X (Code is available upon request).

Maple can't solve DAEs directly. So, the algebraic equations are differentiated and then solved using consistent initial condition found from Leastsquare minimization of residues. There are more robust approaches for solving battery models [M. T. Lawder, V. Ramadesigan, B. Suthar and V. R.

Subramanian, "Extending explicit and linearly implicit ODE solvers for index-1 DAEs", *Computers and Chemical Engineering*, 82, 283-292 (2015). USPTO 10769236].

Running the same code in C using SUNDIALS IDA will be 2 orders of magnitude faster.

Cycling codes (without documentation) is plotted here.

[The equations below are the set of equations after transformation to non dimensional form.

[Governing Equations

[Equation for potential after Landau Transformation

> eq := (diff(c(Z, tau), Z) * diff(phi(Z, tau), Z) + c(Z, tau) * diff(phi(Z, tau), Z\$2)) / (1 - S(tau))^2 = 0;

$$eq := \frac{\left(\frac{\partial}{\partial Z} c(Z, \tau)\right) \left(\frac{\partial}{\partial Z} \phi(Z, \tau)\right) + c(Z, \tau) \left(\frac{\partial^2}{\partial Z^2} \phi(Z, \tau)\right)}{(1 - S(\tau))^2} = 0 \quad (1)$$

[Equation for concentration after Landau transformation

> ceq := diff(c(Z, tau), tau) = -Pe / tD * CC[0] (tau)^.5 * (Va(tau) - UU[0] (tau)) * (1 - Z) / (1 - S(tau)) * diff(c(Z, tau), Z) + diff(c(Z, tau), Z\$2) / (tD * (1 - S(tau))^2);

$$ceq := \frac{\partial}{\partial \tau} c(Z, \tau) = - \frac{Pe \sqrt{CC_0(\tau)} (Va(\tau) - UU_0(\tau)) (1 - Z) \left(\frac{\partial}{\partial Z} c(Z, \tau)\right)}{tD (1 - S(\tau))} + \frac{\frac{\partial^2}{\partial Z^2} c(Z, \tau)}{tD (1 - S(\tau))^2} \quad (2)$$

[Boundary Conditions

Boundary condition for potential at X=0

```
> bc1:=diff(phi(Z,tau),Z)/(1-S(tau))=-Da/c(Z,tau)^.5*(Va(tau)-phi(Z,tau));
```

$$bc1 := \frac{\frac{\partial}{\partial Z} \phi(Z, \tau)}{1 - S(\tau)} = -\frac{Da (Va(\tau) - \phi(Z, \tau))}{\sqrt{c(Z, \tau)}} \quad (3)$$

Boundary conditions for concentration at X=0

```
> cbc1:=diff(c(Z,tau),Z)/(1-S(tau))=-Da*c(Z,tau)^.5*(Va(tau)-phi(Z,tau))+cv*Pe*c(Z,tau)^1.5*(Va(tau)-phi(Z,tau));
```

$$cbc1 := \frac{\frac{\partial}{\partial Z} c(Z, \tau)}{1 - S(\tau)} = -Da \sqrt{c(Z, \tau)} (Va(\tau) - \phi(Z, \tau)) + cv Pe c(Z, \tau)^{1.5} (Va(\tau) - \phi(Z, \tau)) \quad (4)$$

Boundary condition for potential at X=1

```
> bc2:=c(Z,tau)*diff(phi(Z,tau),Z)=-delta*(1-S(tau));
```

$$bc2 := c(Z, \tau) \left(\frac{\partial}{\partial Z} \phi(Z, \tau) \right) = -\delta (1 - S(\tau)) \quad (5)$$

Boundary condition for concentration at X=1

```
> cbc2:=diff(c(Z,tau),Z)=-delta*(1-S(tau));
```

$$cbc2 := \frac{\partial}{\partial Z} c(Z, \tau) = -\delta (1 - S(\tau)) \quad (6)$$

List of parameters

MV = Mw/rho

```
> pars0:=[iapp=10, i0=20,i0cathode=20, D1=1e-11, F= 96487, R=8.314, T=298, Lx=50e-6, c0=1000, MV= 1.2998e-5];
```

```
pars0 := [iapp = 10, i0 = 20, i0cathode = 20, D1 = 1. × 10-11, F = 96487, R = 8.314, T = 298, Lx = 0.000050, c0 = 1000, MV = 0.000012998] \quad (7)
```

Dimensionless groups

```
> pars:=subs(pars0, [delta=iapp*Lx*Crate/2/F/D1/c0, tD=abs(Crate)*Lx^2/(3600*D1), Da=i0*Lx/(2.*F*D1*c0), Pe=MV*i0*Lx/(D1*F), phi0=R*T/F]);
```

```
pars := [\delta = 0.2591022625 Crate, tD = 0.06944444444 |Crate|, Da = 0.5182045250, Pe = 0.01347124483, \phi0 = 0.02567778043] \quad (8)
```

Discretizing the equations using finite difference

Input number of node points

```
> N1:=10;
```

```
NI := 10 \quad (9)
```

Node spacing

```
> h:=1.0/(N1+1);
```

(10)

$$h := 0.09090909091 \quad (10)$$

The variables of c and phi are renamed to be u1 and u2, where u1 = c, u2 = phi

```
> #u1 = C, u2 = phi #
```

```
eq
```

```
> for i from 1 to N1 do:
```

```
  eq11[i] := (u1[i+1](tau) - u1[i-1](tau)) / (2*h) * (u2[i+1](tau) - u2[i-1](tau)) / (2*h) / (-1+S(tau))^2 + u1[i](tau) * (u2[i-1](tau) - 2*u2[i](tau) + u2[i+1](tau)) / h^2 / (-1+S(tau))^2 = 0;
```

```
od:
```

Discretized boundary conditions

```
bc1
```

```
> eq11[0] := (-3*u2[0](tau) + 4*u2[1](tau) - u2[2](tau)) / (2*h) = -1*Da*(Va(tau) - u2[0](tau)) * (1-S(tau)) / u1[0](tau)^.5;
```

$$eq11_0 := -16.50000000 u_{2_0}(\tau) + 22.00000000 u_{2_1}(\tau) - 5.500000000 u_{2_2}(\tau) = \frac{Da (Va(\tau) - u_{2_0}(\tau)) (1 - S(\tau))}{\sqrt{u_{1_0}(\tau)}} \quad (11)$$

```
bc2
```

```
> eq11[N1+1] := (-3*u2[N1+1](tau) + 4*u2[N1](tau) - u2[N1-1](tau)) / (2*h) = -1*delta*(1-S(tau)) / u1[N1+1](tau);
```

$$eq11_{11} := -16.50000000 u_{2_{11}}(\tau) + 22.00000000 u_{2_{10}}(\tau) - 5.500000000 u_{2_9}(\tau) = -\frac{\delta (1 - S(\tau))}{u_{1_{11}}(\tau)} \quad (12)$$

```
ceq
```

```
> ceq;
```

$$\frac{\partial}{\partial \tau} c(Z, \tau) = -\frac{Pe \sqrt{CC_0(\tau)} (Va(\tau) - UU_0(\tau)) (1 - Z) \left(\frac{\partial}{\partial Z} c(Z, \tau) \right)}{tD (1 - S(\tau))} + \frac{\frac{\partial^2}{\partial Z^2} c(Z, \tau)}{tD (1 - S(\tau))^2} \quad (13)$$

```
> for i from 1 to N1 do:
```

```
  eq21[i] := diff(u1[i](tau), tau) = Pe/tD*u1[0](tau)^.5*(u2[0](tau) - Va(tau)) * (1-i*h) / (2*h) * (u1[i+1](tau) - u1[i-1](tau)) / (1-S(tau)) + (u1[i-1](tau) - 2*u1[i](tau) + u1[i+1](tau)) / h^2 / (tD*(1-S(tau))^2); od:
```

```
cbc1
```

```
> eq21[0] := (-3*u1[0](tau) + 4*u1[1](tau) - u1[2](tau)) / (2*h) = (-Da*u1[0](tau)^.5*(Va(tau) - u2[0](tau)) + cv*Pe*u1[0](tau)^1.5*(Va(tau) - u2[0](tau))) * (1-S(tau));
```

$$eq21_0 := -16.50000000 u_{1_0}(\tau) + 22.00000000 u_{1_1}(\tau) - 5.500000000 u_{1_2}(\tau) = \left(\quad (14)$$

$$-Da \sqrt{ul_0(\tau)} (Va(\tau) - u_{2_0}(\tau)) + cv Pe ul_0(\tau)^{1.5} (Va(\tau) - u_{2_0}(\tau)) (1 - S(\tau))$$

cbc2

```
> eq21[N1+1] := (-3*u1[N1+1](tau) + 4*u1[N1](tau) - u1[N1-1](tau)) / (2*h) =
    -delta*(1-S(tau));
eq2l11 := -16.50000000 ul11(tau) + 22.00000000 ul10(tau) - 5.500000000 ul9(tau) = -delta(1
    - S(tau))
```

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Reference electrode potential

```
> Va(tau) := 0;
Va(tau) := 0
```

(16)

Moving boundary velocity

```
> eqz1 := diff(S(tau), tau) = -Pe/tD*(Va(tau) - u2[0](tau))*u1[0](tau)
    ^0.5;
eqz1 := d/dtau S(tau) = (Pe u2_0(tau) sqrt(ul_0(tau))) / tD
```

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Switch to enable/disable the convective term in the boundary equation cbc1

cv = 1 : enable / 0 : disable

```
> cv:=1;
cv := 1
```

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Separating the Ordinary Differential Equations (ODEs) and the Algebraic Equations (AEs)

```
> eqodes := subs(pars, pars0, [seq(eq21[i], i=1..N1), eqz1]);
> eqaes := subs(pars, pars0, [seq(eq11[i], i=0..N1+1), eq21[0], eq21
    [N1+1]]);
> eqaes := map(rhs-lhs, eqaes);
> eqaes2 := subs(eqodes, diff(eqaes, tau));
```

List of variables

```
> aevars := [seq(u2[i](tau), i=0..N1+1), u1[0](tau), u1[N1+1](tau)];
> odevars := [seq(u1[i](tau), i=1..N1), S(tau)];
> aesubs := [seq(aevars[i]=ZZ[i], i=1..nops(aevars))];
```

```
> single_phase := proc(cycle, phase) :
    global sol, dsol;
    local i, rate, icodes, eqic, solic, icaes, ics;
    if phase = c then rate := 1;
    elif phase = d then rate := -1;
    fi;
```

```

if cycle = 1 and phase = c then icores:=[seq(u1[i](tau)=1,i=1..
N1),S(tau)=.02]:
elif phase = c then icores:=[seq(odevars[i]=subs(sol[cycle-1,d],
odevars[i]),i=1..N1+1)]:
else
            icores:=[seq(odevars[i]=subs(sol[cycle  ,c],
odevars[i]),i=1..N1+1)]:
fi:
eqic:=subs(icores,aesubs,Crate=rate,eqaes):
solic:=Optimization:-LSSolve(eqic):
icaes:=subs(solic[2],aesubs):
ics:=op(subs(tau=0,icores)),op(subs(tau=0,icaes)):
dsol:=dsolve({op(subs(Crate=rate,eqodes)),op(subs(Crate=rate,
eqaes2))},ics),type=numeric,implicit=true,maxfun=0,stiff=true,
compile=true):
sol[cycle,phase]:=dsol(1):
end proc:

```

```

> makeplot:=proc(cycle,phase)
global p1,p2,p3,p4,p5;
local offset;
if phase = d then offset:=1; else offset:=0; fi:
p1[cycle,phase]:=plots:-odeplot(dsol,[(2*(cycle-1)+offset+tau)*
3600,u1[ 0](tau)*1000],0..1,axes=boxed,legend= C_at_MB ,
thickness=3,color=red ):
p2[cycle,phase]:=plots:-odeplot(dsol,[(2*(cycle-1)+offset+tau)*
3600,u1[N1+1](tau)*1000],0..1,axes=boxed,legend= C_at_top,
thickness=3,color=blue):
p3[cycle,phase]:=plots:-odeplot(dsol,[(2*(cycle-1)+offset+tau)*
3600,u2[ 0](tau)      ],0..1,axes=boxed,legend=Phi_at_MB ,
thickness=3,color=red ):
p4[cycle,phase]:=plots:-odeplot(dsol,[(2*(cycle-1)+offset+tau)*
3600,u2[N1+1](tau)      ],0..1,axes=boxed,legend=Phi_at_top,
thickness=3,color=blue):
p5[cycle,phase]:=plots:-odeplot(dsol,[(2*(cycle-1)+offset+tau)*
3600,      S(tau)*50  ],0..1,axes=boxed,thickness=3,color=red):
print(Cycle=cycle,Phase=phase,ended);
end proc:

```

```

> runcycle:=proc(cycle)
global pc,pphi,pmb;
local i;
for i from 1 to cycle do

```

```

single_phase(i,c);
    makeplot(i,c);
single_phase(i,d);
    makeplot(i,d);
od:

pc :=plots:-display({seq(op([p1[i,c],p1[i,d],p2[i,c],p2[i,d]]),
i=1..testcycle)},title="Li Concentration during charging phase",
    labels=["time [seconds]","Li concentration
[mol/m^3]"],labeldirections=[horizontal, vertical]):
pphi:=plots:-display({seq(op([p3[i,c],p3[i,d],p4[i,c],p4[i,d]]),
i=1..testcycle)},title="Electrolyte potential during charging
phase",
    labels=["time [seconds]","Potential [V]"],
labeldirections=[horizontal, vertical]):
pmb :=plots:-display({seq(op([p5[i,c],p5[i,d]]),i=1..testcycle)},
title="Li Electrode Thickness during charging phase",
    labels=["time [seconds]","Thickness [1e-6 m]
"],labeldirections=[horizontal, vertical]):
print("simulation complete"):
end proc:

```

```
> testcycle:=10;
```

```
testcycle := 10
```

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```
> runcycle(testcycle);
```

```

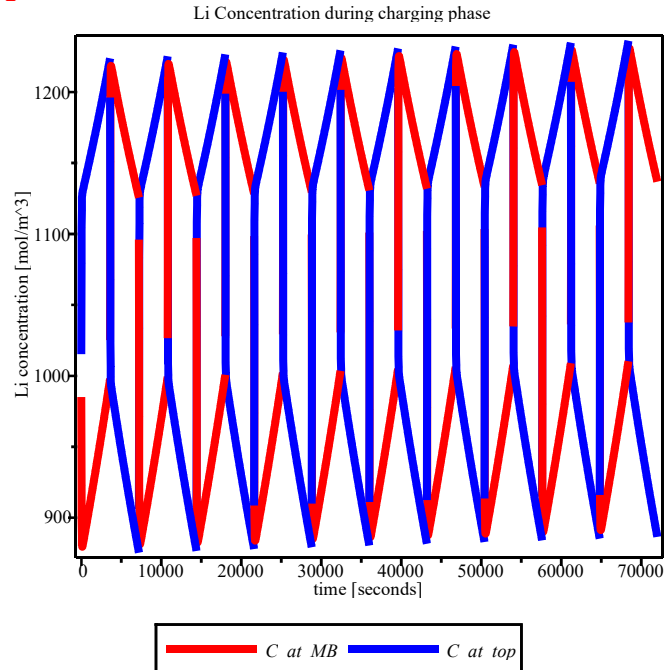
Cycle = 1, Phase = c, ended
Cycle = 1, Phase = d, ended
Cycle = 2, Phase = c, ended
Cycle = 2, Phase = d, ended
Cycle = 3, Phase = c, ended
Cycle = 3, Phase = d, ended
Cycle = 4, Phase = c, ended
Cycle = 4, Phase = d, ended
Cycle = 5, Phase = c, ended
Cycle = 5, Phase = d, ended
Cycle = 6, Phase = c, ended
Cycle = 6, Phase = d, ended
Cycle = 7, Phase = c, ended
Cycle = 7, Phase = d, ended
Cycle = 8, Phase = c, ended
Cycle = 8, Phase = d, ended
Cycle = 9, Phase = c, ended

```

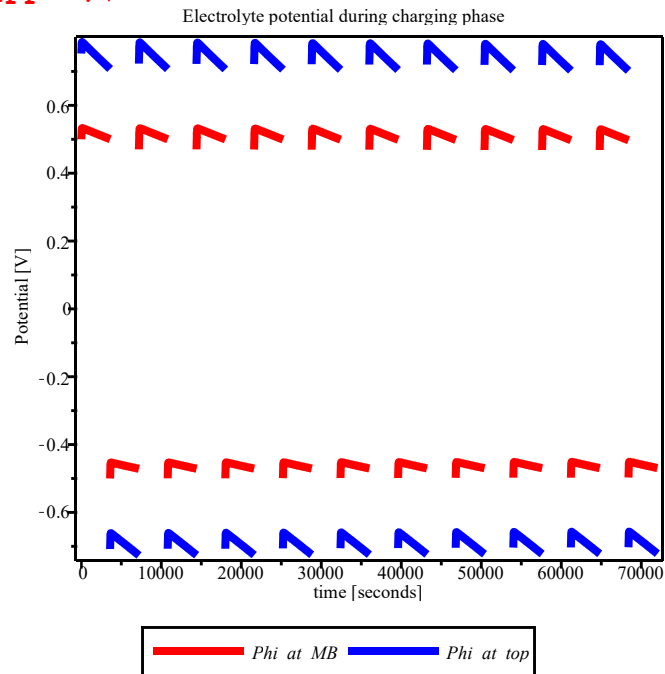
Cycle = 9, Phase = d, ended
Cycle = 10, Phase = c, ended
Cycle = 10, Phase = d, ended
"simulation complete"

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```
> plots:-display(pc) ;
```



```
> plots:-display(pphi) ;
```



```
> plots:-display(pmb) ;
```

Li Electrode Thickness during charging phase

